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**AMENDMENTS TO THE CLAIMS**

This listing of the claims will replace all prior versions and listings of claims in the application:

1. (Original) A process to improve dewaxing performance and extraction yields of a lube boiling range stream comprising:
  - a) contacting a light lube stream in a first solvent extraction zone with a first extraction solvent to produce at least a first aromatics-rich extract solution and a first aromatics-lean raffinate solution;
  - b) removing at least a portion of said first extraction solvent from said first aromatics-rich extract solution to produce at least a first aromatics-rich extract;
  - c) mixing at least a portion of said first aromatics-rich extract with a heavier lube stream to produce a mixed lube stream;
  - d) contacting said mixed lube stream in a second solvent-extraction zone with a second extraction solvent to produce at least a second aromatics-rich extract solution and a second aromatics-lean raffinate solution;
  - e) removing at least a portion of said second extraction solvent from said second aromatics-lean raffinate solution to produce at least a second aromatics-lean raffinate; and
  - f) dewaxing said second aromatics-lean raffinate to produce at least one base oil.

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2. (Original) The process of claim 1 wherein said light lube stream is characterized as having a mid boiling point range of about 350°C to about 450°C.

3. (Original) The process according to claim 2 wherein said heavier lube stream has a mid boiling point range greater than 450°C.

4. (Original) The process of claim 3 wherein said light lube stream is a hydrocracked light lube stream.

5. (Original) The process of claim 4 wherein said first extraction solvent and said second extraction solvent are selected from the group consisting of sulfolane, furfural, phenol, and N-methyl pyrrolidone (NMP).

6. (Original) The process of claim 5 wherein at least about 5 volume percent of said first aromatics-rich extract is conducted to said mixing zone.

7. (Original) The process of claim 6 wherein at least about 25 volume percent of said first aromatics-rich extract is conducted to said mixing zone.

8. (Original) The process of claim 7 wherein at least about 35 volume percent of said first aromatics-rich extract is conducted to said mixing zone.

9. (Original) The process according to claim 8 wherein the mixed lube stream comprises less than about 70 volume percent, based on the mixed lube stream, of the first aromatics-rich extract.

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10. (Original) The process according to claim 9 wherein the mixed lube stream comprises less than about 30 volume percent, based on the mixed lube stream, of the first aromatics-rich extract.

11. (Original) The process according to claim 10 wherein the mixed lube stream comprises about 15 volume percent, based on the mixed lube stream, of the first aromatics-rich extract.

12. (Original) The process of claim 5 wherein said second aromatics-lean raffinate is dewaxed in a catalytic dewaxing zone.

13. (Original) The process according to claim 5 wherein said second aromatic-lean raffinate is dewaxed in a solvent dewaxing zone.

14. (Original) The process of claim 13 wherein said at least one base oil is characterized as having a mid-boiling point range (50% LV), as determined by ASTM D6417, of about 400 to about 490°C, and a Viscosity Index of about 80-120.

15. (Original) The base oil of claim 14.

16. (Original) The process of claim 13 wherein said heavier lube stream is a hydrocracked heavier lube stream.

17. (Original) A process to improve dewaxing performance and extraction yields of a lube boiling range stream comprising:

- a) contacting at least one light lube stream in a first solvent extraction zone with a first extraction solvent to produce at least

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a first aromatics-rich extract solution and a first aromatics-lean raffinate solution;

b) removing at least a portion of said first extraction solvent from said first aromatics-rich extract solution to produce at least a first aromatics-rich extract;

c) contacting at least one other light lube stream in a second solvent extraction zone with a second extraction solvent to produce at least a second aromatics-rich extract solution and at least a second aromatics-lean raffinate solution;

d) removing at least a portion of said second extraction solvent from said second aromatics-rich extract solution to produce at least a second aromatics-rich extract;

e) mixing at least a portion of said first aromatics-rich extract and at least a portion of said second aromatics-rich extract with a heavier lube stream to produce a mixed lube stream;

f) contacting said mixed lube stream in a solvent-extraction zone with a third extraction solvent to produce at least a third aromatics-rich extract solution and at least a third aromatics-lean raffinate solution;

g) removing at least a portion of said third extraction solvent from said third aromatics-lean raffinate solution to produce at least a first aromatics-lean raffinate;

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h) dewaxing said third aromatics-lean raffinate to produce at least one base oil.

18. (Original) The process according to claim 17 wherein said at least one light lube stream is a hydrocracked light lube stream and said at least one other light lube stream is a hydrocracked light lube stream.

19. (Original) The process according to claim 18 wherein said third aromatics-lean raffinate is dewaxed in said dewaxing zone by the use of solvent dewaxing methods or processes.

20. (Original) The process according to claim 19 wherein there exists more than two light lube streams that are hydrocracked light lube streams, hydrotreated light lube streams, or any combination thereof.

21. (Original) The process according to claim 20 wherein said heavier lube stream is a heavier hydrocracked lube stream.

22. (Original) The process according to claim 20 wherein said first aromatics-lean extract and said second aromatics-lean extract are mixed prior to being mixed in the mixing zone with the heavier lube stream.

23. (Canceled)